Couette flow with applied pressure gradient $\vec{n} \cdot \vec{n} = \vec{n} \cdot \vec{n} \cdot \vec{n} + \vec{n} \cdot \vec{n} \cdot \vec{n} + \vec{n} \cdot \vec{n} \cdot \vec{n} = \vec{n}$ The same as in the Couette flow of the previous slides but the x-component of the momentum equation is r_{c} Moving plate now: $M = \sqrt{R}$ $\int_{T}^{T} + \frac{1}{2} \sqrt{2} \sqrt{R}$ $= -\sqrt{R} + \sqrt{2} \sqrt{2} \sqrt{2} \sqrt{2}$ now: Fluid: ρ , μ Fixed plate $\frac{\partial P}{\partial x} + \frac{\partial \nabla^2 M}{\partial x} = 0$ Result of x-momentum: $\frac{\partial P}{\partial r} = \frac{P_2 - P_1}{r_2 - r_1}$ (x_1) $\frac{d^2u}{dv^2} = \frac{1}{\mu} \frac{\partial P}{\partial x}$ Integrating twice yields $u = \frac{1}{2\mu} \frac{\partial P}{\partial x} y^2 + C_1 y + C_2 \qquad \begin{cases} \frac{\partial P}{\partial x} = \frac{\partial f}{\partial x} = C_T e \\ \frac{\partial P}{\partial x} = \frac{\partial P}{\partial x} \\ f = (\frac{\partial P}{\partial x}) \cdot \mathcal{K} + P_0 \end{cases}$ Integration of x-momentum: For the pressure Integration of z-momentum: $P = -\rho gz + f(x)$ $P = P_0 + \frac{\partial P}{\partial x}x - \rho gz$ Final result for pressure field:

Applying the velocity boundary conditions

$$u = \frac{1}{2\mu} \frac{\partial P}{\partial x} \times 0 + C_1 \times 0 + C_2 = 0 \quad \Rightarrow \quad \underline{C_2 = 0} \quad (= \mathcal{M}(\mathcal{G} = 0) = 0)$$

$$u = \frac{1}{2\mu} \frac{\partial P}{\partial x} h^2 + C_1 \times h + 0 = V \quad \Rightarrow \quad C_1 = \frac{V}{h} - \frac{1}{2\mu} \frac{\partial P}{\partial x} h \quad (= \mathcal{M}(\mathcal{G} = h)) = \sqrt{2}$$

$$u = \frac{Vy}{h} + \frac{1}{2\mu} \frac{\partial P}{\partial x} (y^2 - hy)$$

• u(y) is the velocity profile of Couette flow between parallel plates with an applied negative pressure gradient; the dashed red line indicates the profile for a zero pressure gradient, and the dotted line indicates the profile for a negative pressure gradient with the upper plate stationary (V = 0).

х

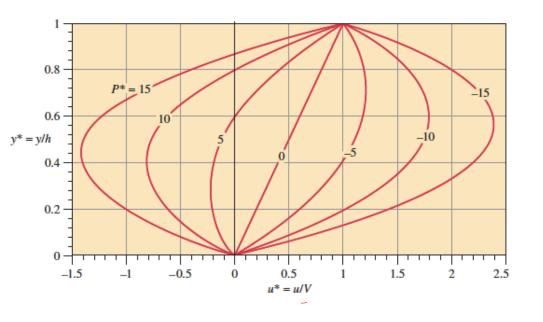
Dimensional analysis

 The problem is set in terms of velocity u as a function of y, h, V, m, and dP/dx. There are six variables (including the dependent variable u), and since there are three primary dimensions (mass, length, and time), we expect 6 - 3 dimensionless groups. When we pick h, V, and m as our repeating variables, we get the following result:

Dimensional analysis

Dimensionless form of velocity field:

$$u^* = y^* + \frac{1}{2}P^*y^*(y^* - 1)$$



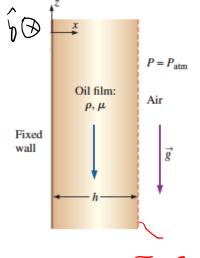
where

$$u^{*} = \frac{u}{V} \quad y^{*} = \frac{y}{h} \quad P^{*} = \frac{h^{2}}{\mu V} \frac{\partial P}{\partial x}$$

SI:
$$y \rightarrow m^{2}/j \quad P \rightarrow N/m^{2}$$
$$M \rightarrow k_{g}/(m-j)$$

35

Oil film falling down a vertical wall



- 1. The wall is infinite in the yz-plane (y is into the page for a right-handed coordinate system).
- $P = P_{atm}$ 2. The flow is steady (all partial derivatives with respect to time are zero).
 Air 3. The flow is parallel (the x-component of velocity, u, is zero everywhere).
 4. The fluid is incompressible and Newtonian with constant properties, and the flow is laminar.
 - 5. Pressure $P = P_{atm}$ constant at the free surface. In other words, there is no applied pressure gradient pushing the flow; the flow establishes itself due to a balance between gravitational forces and viscous forces. In
- $\tau \sim 2^{\circ}$ addition, since there is no gravity force in the horizontal direction, P = P_{atm} everywhere.

6. The velocity field is purely 2D, which implies that derivatives in y are zero.

7. Gravity acts in the negative z direction.

8. The boundary conditions are: no slip at the wall; at x = 0, u = v = w = 0. At the free surface (x = h), there is negligible shear, which for a vertical free surface, in this coordinate system, means $\frac{\partial w}{\partial x} = 0$ at x = h.

Continuity:

$$\begin{array}{c}
\lambda = 0 & \sqrt{2} \cdot 0 \\
\hline y \cdot \overline{x} = 0 & \frac{\partial \phi}{\partial x} + \frac{\partial \psi}{\partial y} + \frac{\partial w}{\partial z} = 0 & \rightarrow & \frac{\partial w}{\partial z} = 0 \\
\hline Result of continuity: & w = w(x) \text{ only} \\
\hline NS w: & p\left(\frac{\partial \psi}{\partial t} + u\frac{\partial \psi}{hx} + v\frac{\partial \psi}{\partial y} + w\frac{\partial \psi}{hz}\right) = -\frac{\partial P}{hz} + pg_{z} \\
& + \mu\left(\frac{\partial^{2}w}{\partial x^{2}} + \frac{\partial^{2}\psi}{\partial y^{2}} + \frac{\partial^{2}\psi}{\partial z^{2}}\right) \rightarrow \left(\frac{d^{2}w}{dx^{2}} = \frac{pg}{\mu}\right) \\
\hline Delta = 0 & 0 & 0 + 0 + C_{2} = 0 \\
\hline w(x = 0) = 0 \\
\hline Boundary condition (1): & w = 0 + 0 + C_{2} = 0 \\
\hline and \\
\hline w(x = h) = 0 \\
\hline Velocity field: & w = \frac{pg}{2\mu}x^{2} - \frac{pg}{\mu}h + C_{1} = 0 \rightarrow C_{1} = -\frac{pgh}{\mu} \\
\hline Velocity field: & w = \frac{pg}{2\mu}x^{2} - \frac{pg}{\mu}hx = \frac{pgx}{2\mu}(x - 2h) \\
\hline Reading for the next class: Cengel, examples 9-18 and 9-19
\end{array}$$