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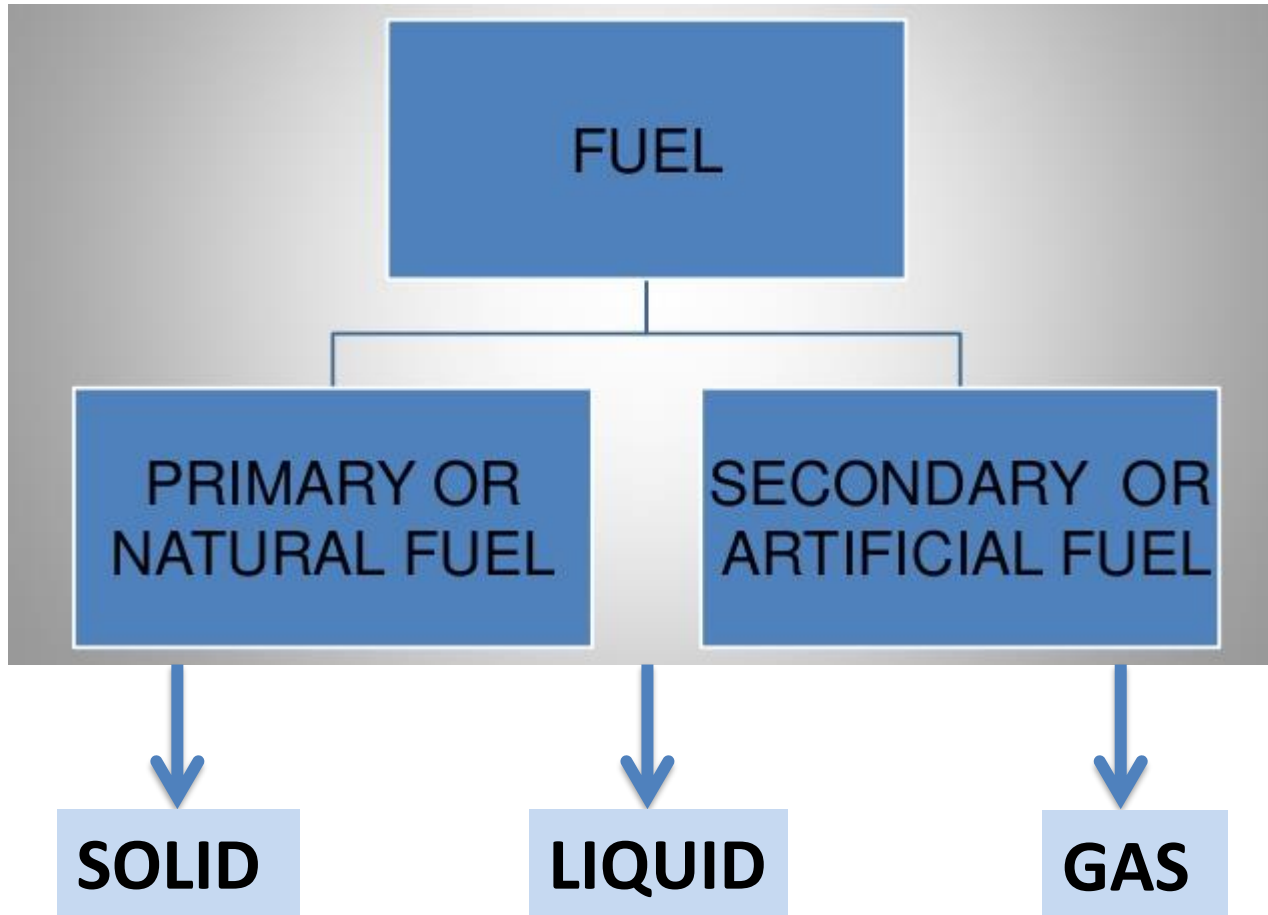
DISCIPLINA MIEA 2019



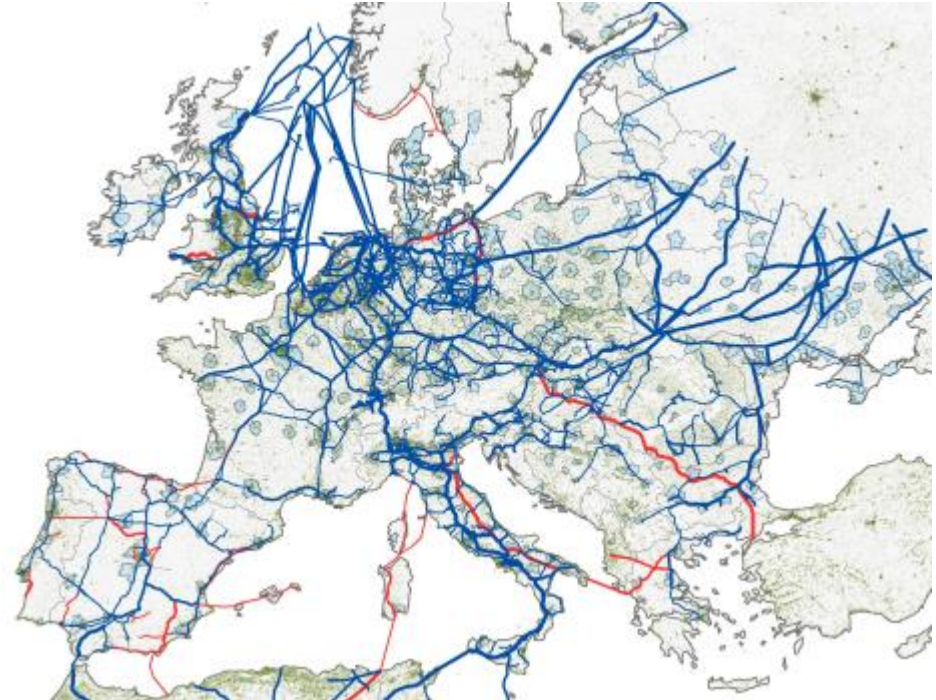
Technologies of combustion

Corpo docente

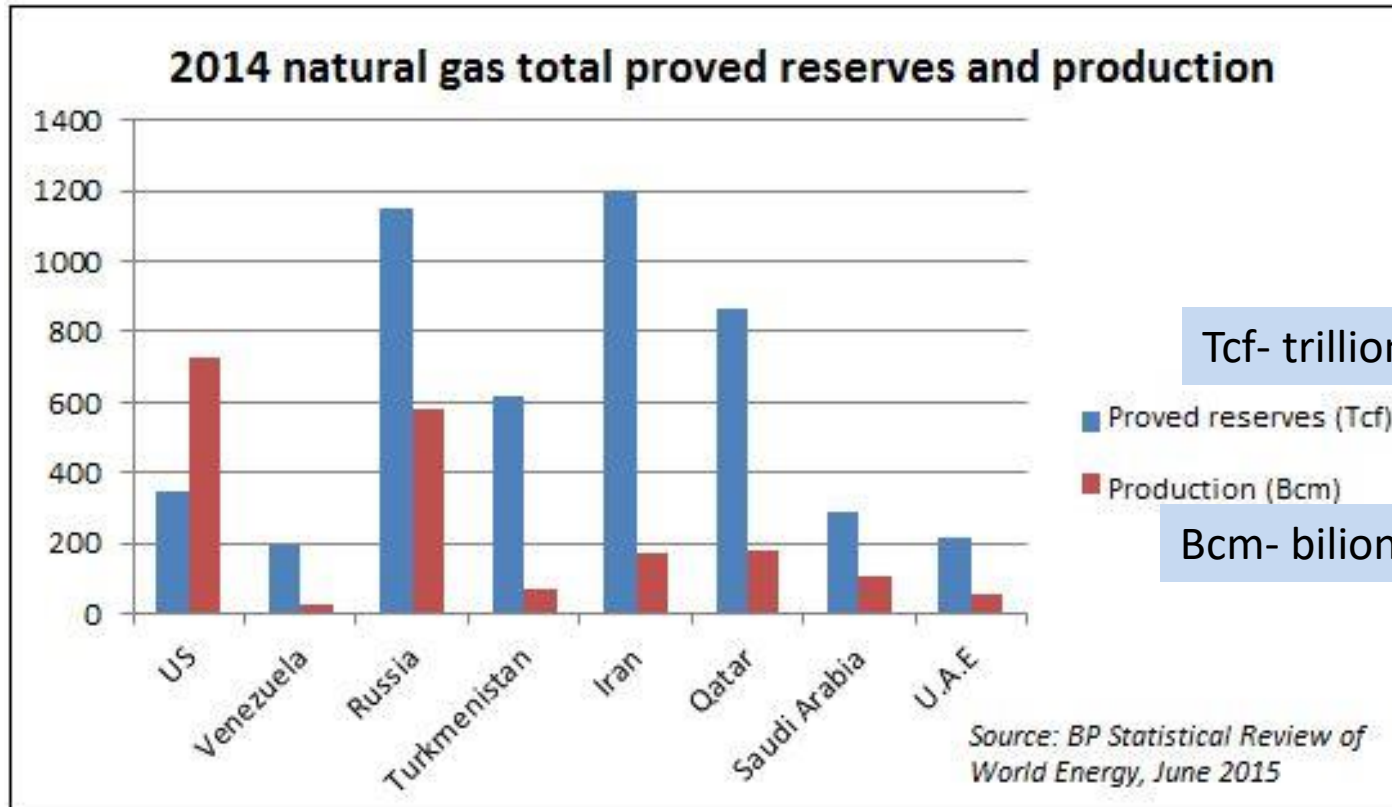
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Natural gas network

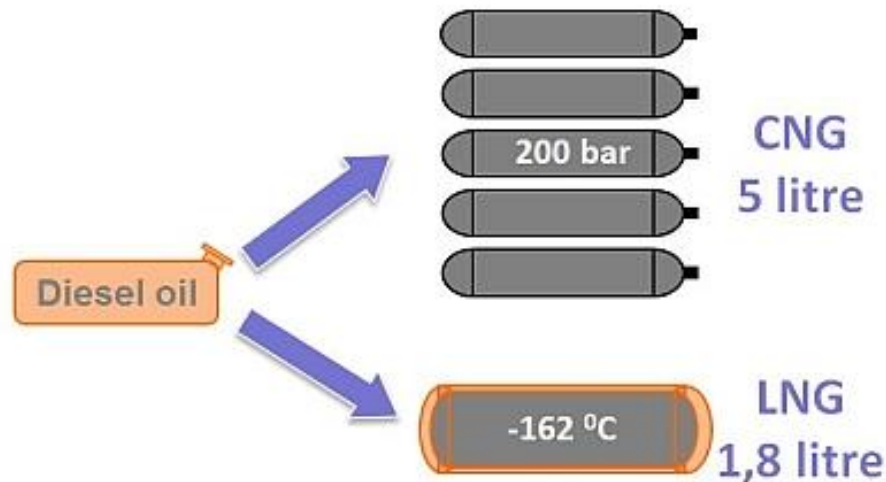


**The European natural gas network.
The existing network is shown in
blue; planned pipelines in red.
Population density is represented in
dark green; larger urban areas are
coloured light blue.
(Image: ETH Zurich)**



Natural gas

Visual comparison of the volumetric equivalence between diesel, CNG, and LNG for a given energy content. (NGVA Europe).



Addition of odorants to help identify NG in case of a leak.

Quality/unit	Natural methane	LPG propane	LPG butane
Chemical formula	CH ₄	C ₃ H ₈	C ₄ H ₁₀
Boiling point	-162°C	-42°C	-2°C
Specific gravity of liquid fuel	-	0.5	0.57
Specific gravity of gas vapour	0.58	1.78	2.0
Gross calorific value	38.5 MJ/m ³	95 MJ/m ³	121.5 MJ/m ³
Gas family	2nd	3rd	3rd
Flammability limits	5–15%	2.3–9.5%	1.9–8.5%
Air/gas ratio	9.81:1	23.8:1	30.9:1
Oxygen/gas ratio	2:1	5:1	6.5:1
Flame speed	0.36 m/s	0.46 m/s	0.38 m/s
Ignition temperature	704°C	530°C	500°C
Max. flame temperature	1000°C	1980°C	1996°C
System operating pressure	21 ± 2 mbar	37 ± 5 mbar	28 ± 5 mbar
Liquid storage vapour pressure	-	6–7 bar	1.5–2 bar



Correlation for natural gas heat capacity developed

Table 1

GAS COMPOSITIONS USED FOR GENERATING C_p VALUES

————— Natural gas mixtures, mole % —————

Component	Gas				
	A	B	C	D	E
CH ₄	94.4	88.9	83.2	78.0	74.9
C ₂ H ₆	2.6	5.2	8.8	10.5	10.1
C ₃ H ₈	2.0	3.7	4.2	6.5	7.2
i-C ₄ H ₁₀	0.5	0.7	1.1	1.5	2.4
n-C ₄ H ₁₀	0.5	0.7	1.1	1.5	2.4
i-C ₅ H ₁₂	0.0	0.4	0.8	1.0	1.5
n-C ₅ H ₁₂	0.0	0.4	0.8	1.0	1.5
Mol wt	17.39	18.83	20.28	21.72	23.18
SG	0.60	0.65	0.70	0.75	0.80

Natural gas network

Biogas		Landfill	Waste water	House	Industrial
		gas	treatment	hold	waste/animal
			digester	waste	manure digester
				digester	
Methane	vol.%	36–52 ^a	65 ^a	65 ^a	60–80/50–70 ^b
Carbon dioxide	vol.%	30–41 ^a	33.5 ^a	29 ^a	20–40/30–50 ^b
Water vapour	vol.%	0.1–3.3 ^a	2 ^a	0.5 ^a	1–4 ^b
Nitrogen	vol.%	<10 ^b	<5 ^b		n.d./<5 ^b
Oxygen	vol.%	<3 ^b	<1 ^b		n.d./<1 ^b
Siloxanes ^c	mg/m ³	1.4–9.8 ^a	1.3 ^a	1.35 ^a	n.d. ^a
Sulphur	mg/m ³	29–900 ^a	<25 ^a	30 ^a	
Hydrogen sulfide	ppm	10–1000 ^b	150–3000		<30000/<5000 ^b
Ammonia	ppm	<5 ^a	<5 ^a	<5 ^a	<5 ^a
Halogenated compounds ^d	mg/m ³	0–7 ^a	n.d.	n.d.	<0.1 ^a
Benzene	mg/m ³	<36 ^e	<0.3 ^e		
Toluene	mg/m ³	<287 ^e	<12 ^e		

^a Arnold [4].

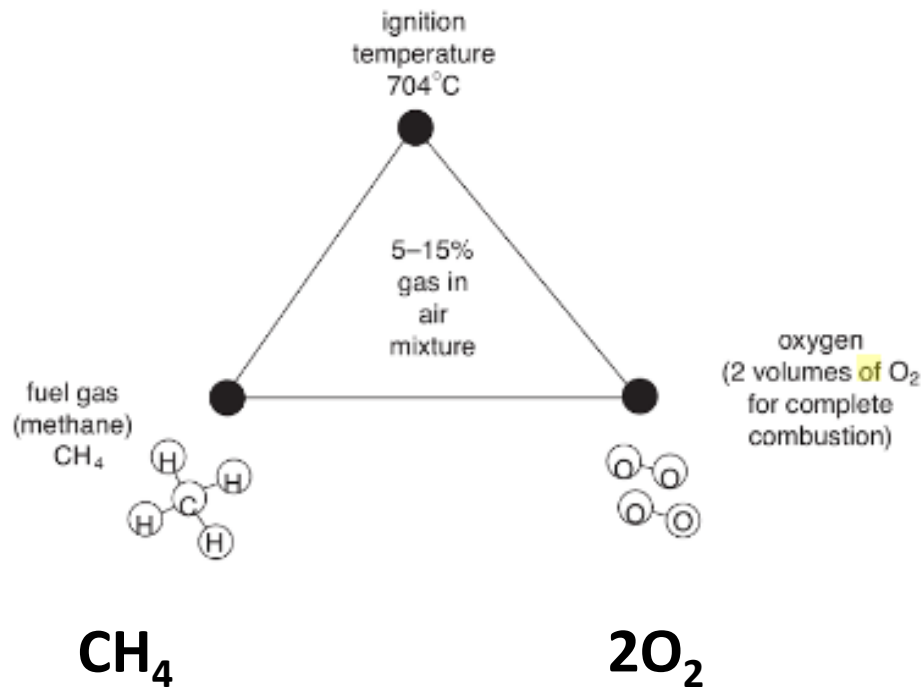
^b Oasmaa and Di Felipe [9].

^c I2–I4, D2–D4, TMS.

^d Quantified as toluene equivalent; n.d. = not detected.

^e Rasi et al. [10].

Methane combustion essentials



Stoichiometry

Natural gas interchangeability

- Appliances
- Boilers
- Burners
- Power plants
- Turbines

$$\text{heat release burner} = kd^2_0 \sqrt{\Delta p} \left(\frac{HV \rho_{fu}}{\sqrt{\frac{\rho_{fu}}{\rho_{air}}}}} \right)$$

Dimensionless
constant

Hole diameter
of the burner

Heat release
throughout the hole



Wobbe Index (WI)

Natural gas interchangeability

Appliances
 Boilers
 Burners
 Power plants
 Turbines

e.g. biogas

Family	Gas type	Approx. Wobbe no.
1st	Manufactured (town gas)	24–29
2nd	Natural	48–53
3rd	LPG	72–87

MJ/Nm³

Gas fuel

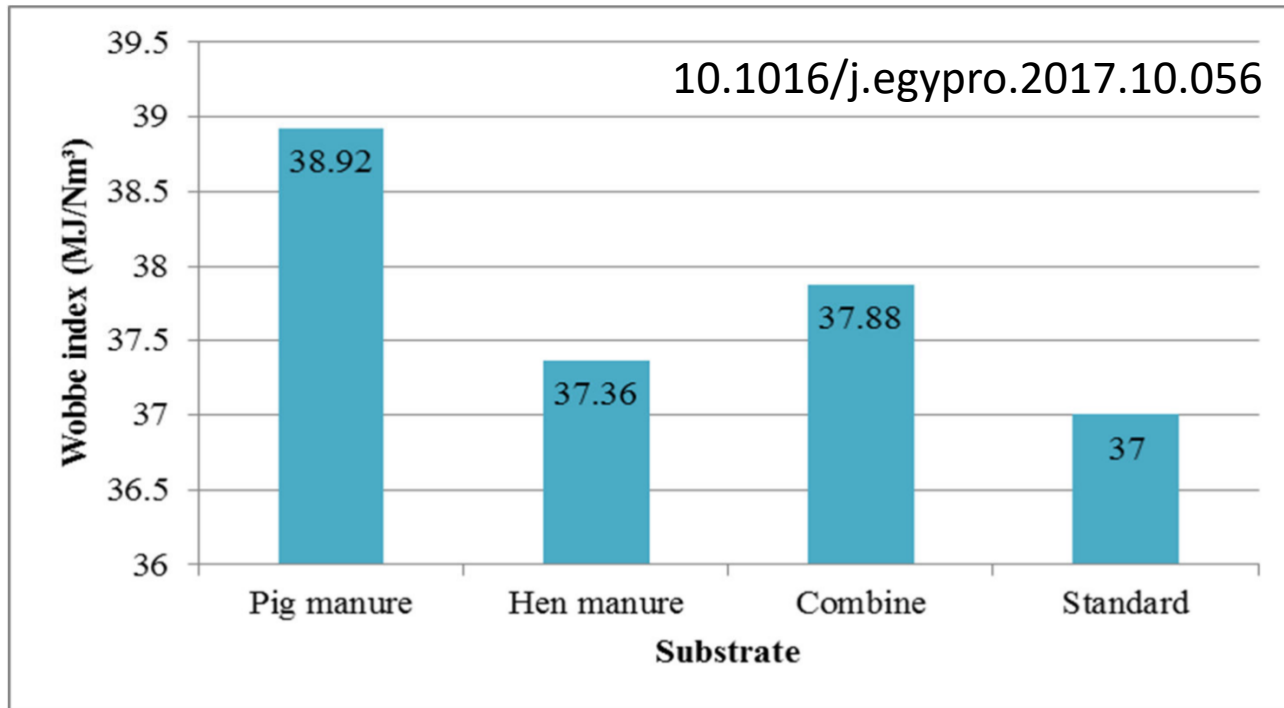


Fig. 2. Wobbe index Comparison in various substrate with standard

e.g. biogas

Family	Gas type	Approx. Wobbe no.
1st	Manufactured (town gas)	24–29
2nd	Natural	48–53
3rd	LPG	72–87

MJ/Nm³

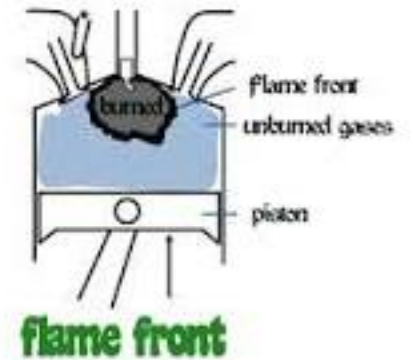
Flame speed

Laminar

Turbulent

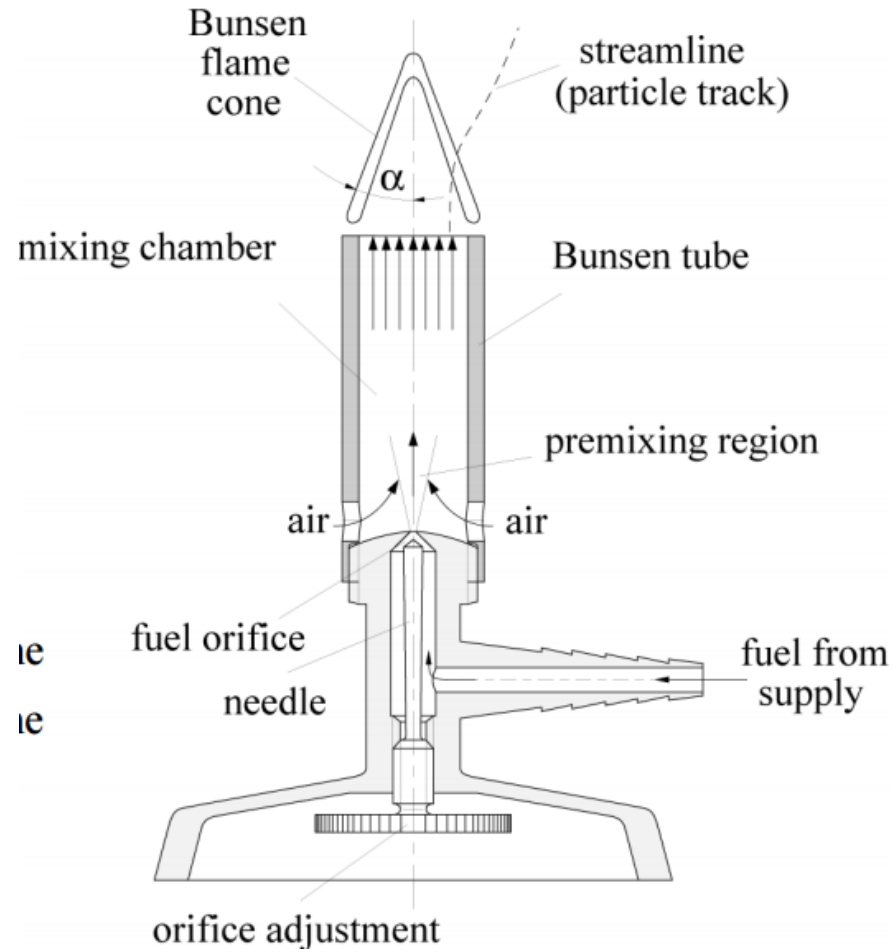


Pre-mixture



Difusion



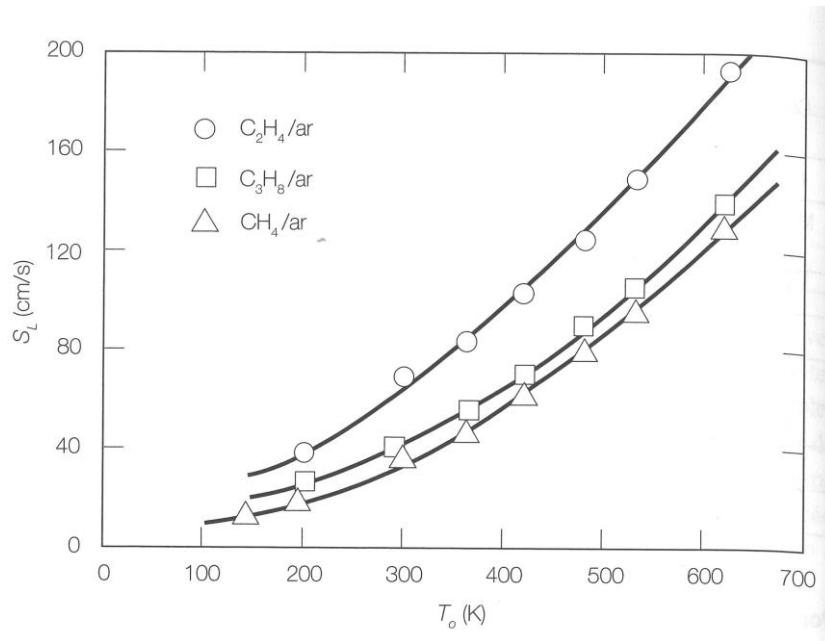


Laminar Flame Speed

$$SL \propto T^m$$

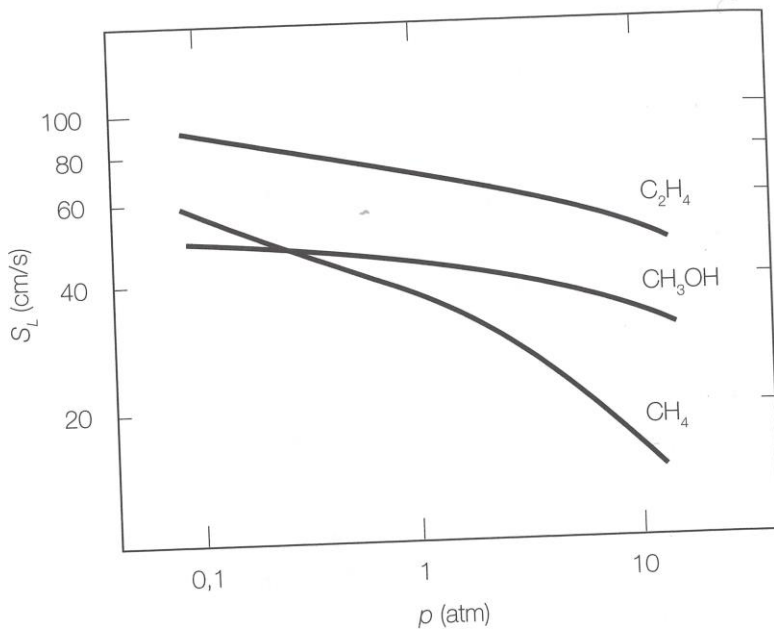


Reactants initial temperature



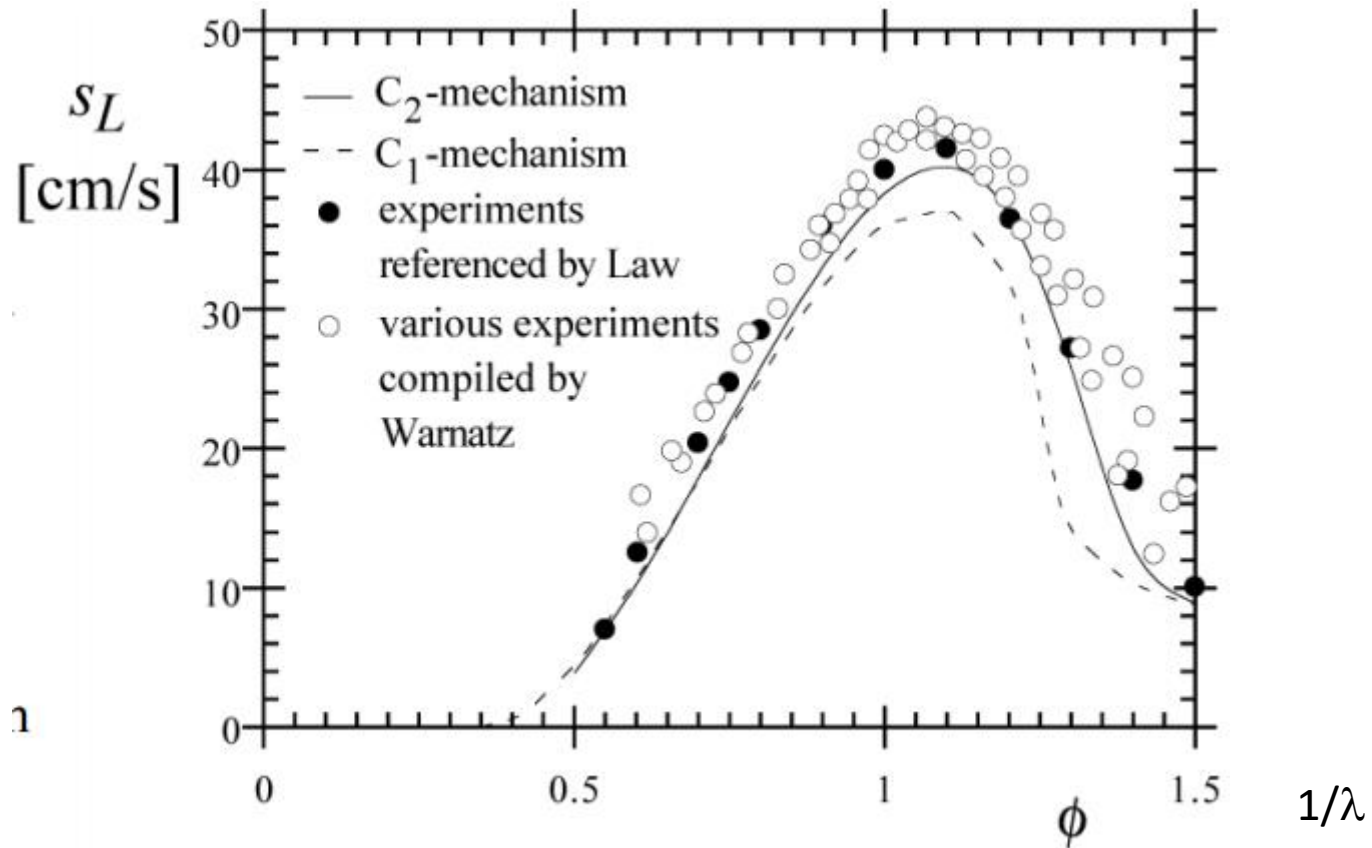
$$SL_{CH_4} \left(\frac{cm}{s} \right) = 10 + 3.71 \times 10^{-4} T^2$$

Laminar Flame Speed



$$SL_{CH_4} \left(\frac{cm}{s} \right) = 43p^{-0.5}$$

p em atm



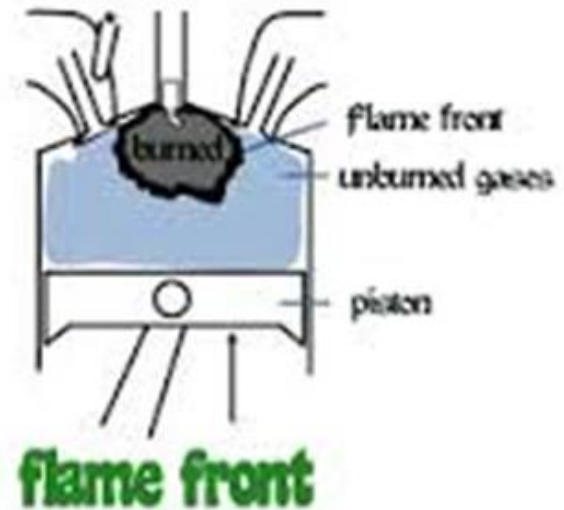
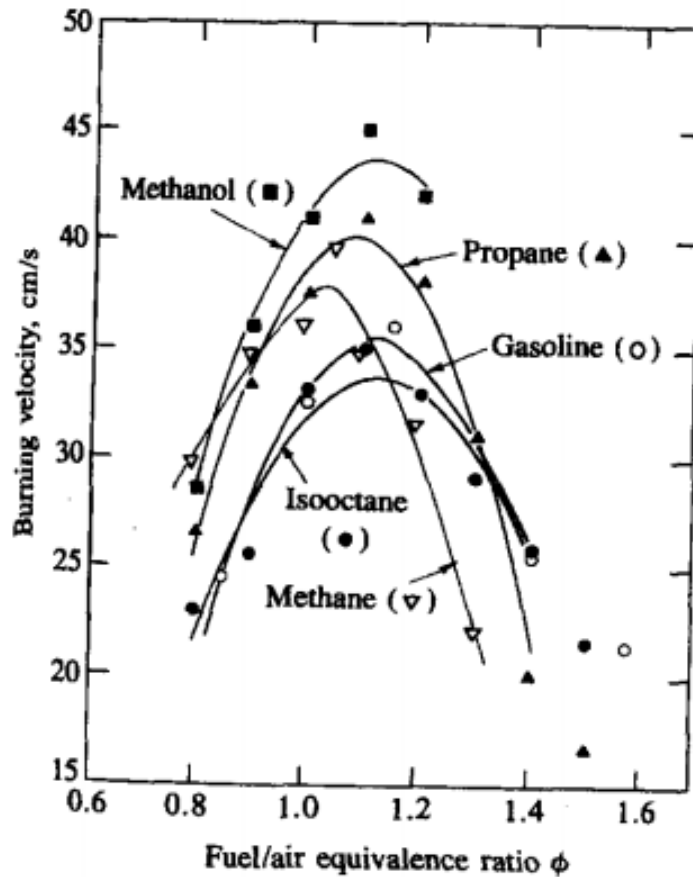


FIGURE 9-25
 Laminar burning velocity for several fuels as function of equivalence ratio, at 1 atm and 300 K. Lines are least-squares polynomial fits to data.^{29, 30}

$$S_L = S_{L,0} \left(\frac{T_u}{T_0} \right)^\alpha \left(\frac{p}{p_0} \right)^\beta \quad (9.33)$$

where $T_0 = 298 \text{ K}$ and $p_0 = 1 \text{ atm}$ are the reference temperature and pressure, and $S_{L,0}$, α , and β are constants for a given fuel, equivalence ratio, and burned gas diluent fraction. For propane, isooctane, and methanol, these constants can be represented by

$$\alpha = 2.18 - 0.8(\phi - 1) \quad (9.34a)$$

$$\beta = -0.16 + 0.22(\phi - 1) \quad (9.34b)$$

and

$$S_{L,0} = B_m + B_\phi(\phi - \phi_m)^2 \quad (9.35)$$

where ϕ_m is the equivalence ratio at which $S_{L,0}$ is a maximum with value B_m .

Parameters ϕ_m , B_m , and B_ϕ for Eq. (9.35)

Fuel	ϕ_m	B_m , cm/s	B_ϕ , cm/s	Ref.
Methanol	1.11	36.9	-140.5	30
Propane	1.08	34.2	-138.7	30
Isooctane	1.13	26.3	-84.7	30
Gasoline	1.21	30.5	-54.9	32

Note: Values of $S_{L,0}$ given by Eq. (9.35) are obtained from least-squares fits of Eq. (9.33) to data over the range $p = 1-8 \text{ atm}$, $T_u = 300-700 \text{ K}$. They do not correspond exactly to the laminar flame speed data at 1 atm and 298 K in Fig. 9-25.

Metghalchi & Keck (1982)

Metghalchi & Keck (1982)

$$S_L = S_{L,ref} \left(\frac{T_o}{T_{o,ref}} \right)^{\alpha_T} \left(\frac{p}{p_{ref}} \right)^{\alpha_p}$$

	$S_{L,ref}$ (m/s)	α_T	α_p
Metano ($\phi = 0,8$)	0,259	2,105	-0,504
Metano ($\phi = 1,0$)	0,360	1,612	-0,374
Metano ($\phi = 1,2$)	0,314	2,000	-0,438
Propano ($0,8 \leq \phi \leq 1,5$)	$0,34 - 1,38 (\phi - 1,08)^2$	$2,18 - 0,8 (\phi - 1)$	$-0,16 + 0,22 (\phi - 1)$

$1/\lambda$

Turbulence effect

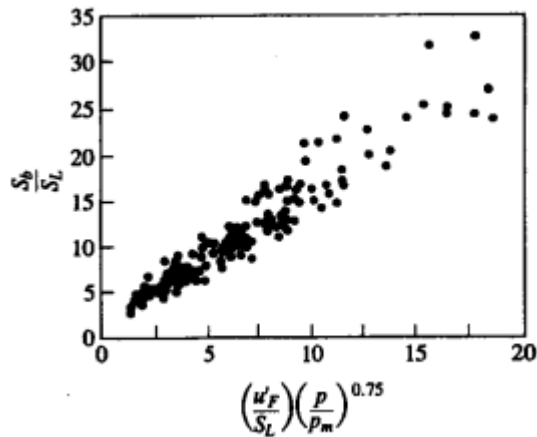
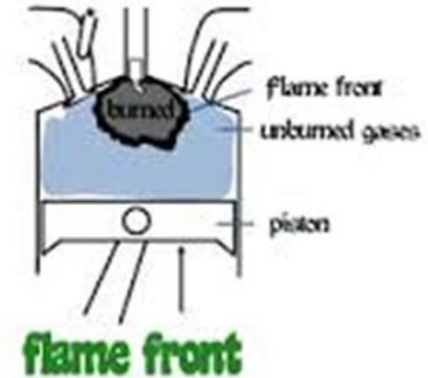
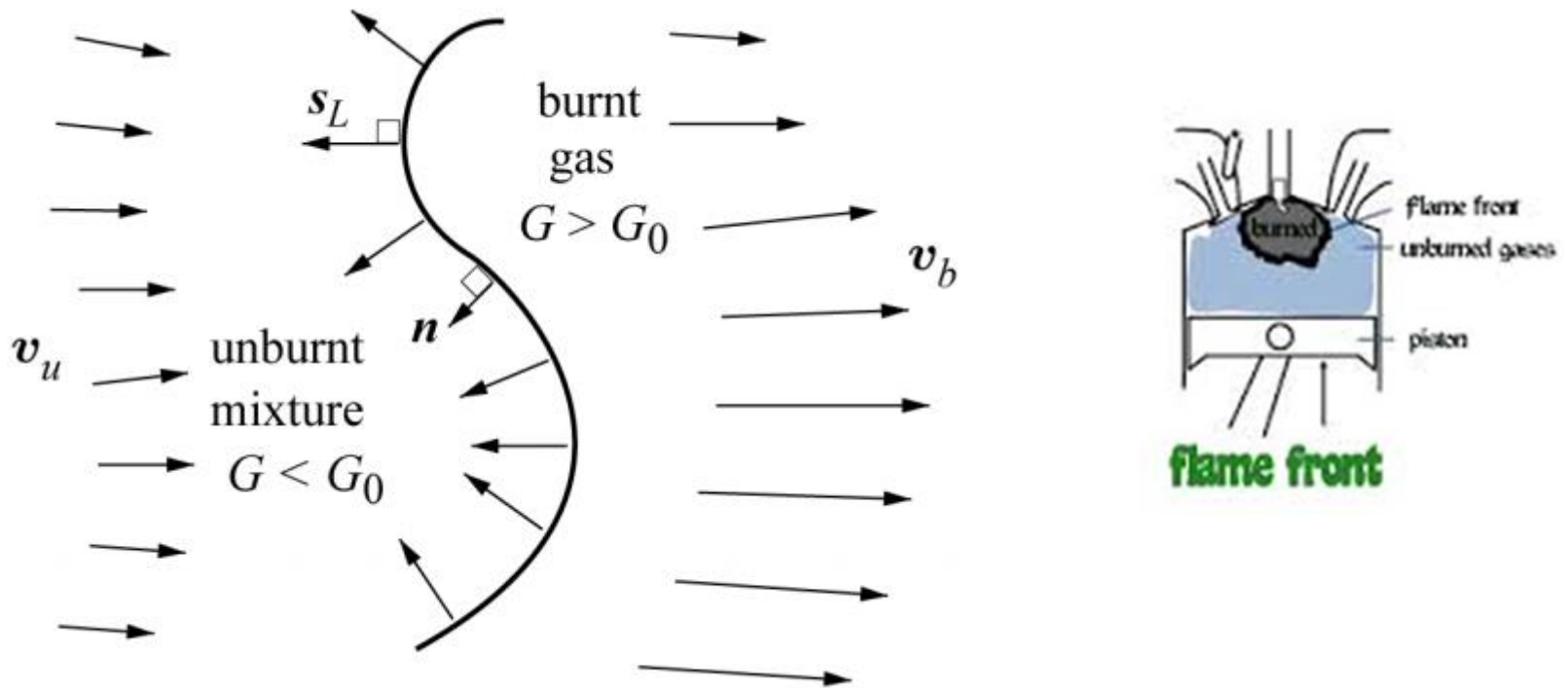


FIGURE 9-30

Variation of burning speed with turbulence intensity. The ensemble-averaged rms velocity fluctuation was measured during motoring engine operation. The ratio p/p_m (firing pressure/motoring pressure) corrects for the effect of additional compression on the turbulence intensity. Range of engine speeds and spark timings.³⁵

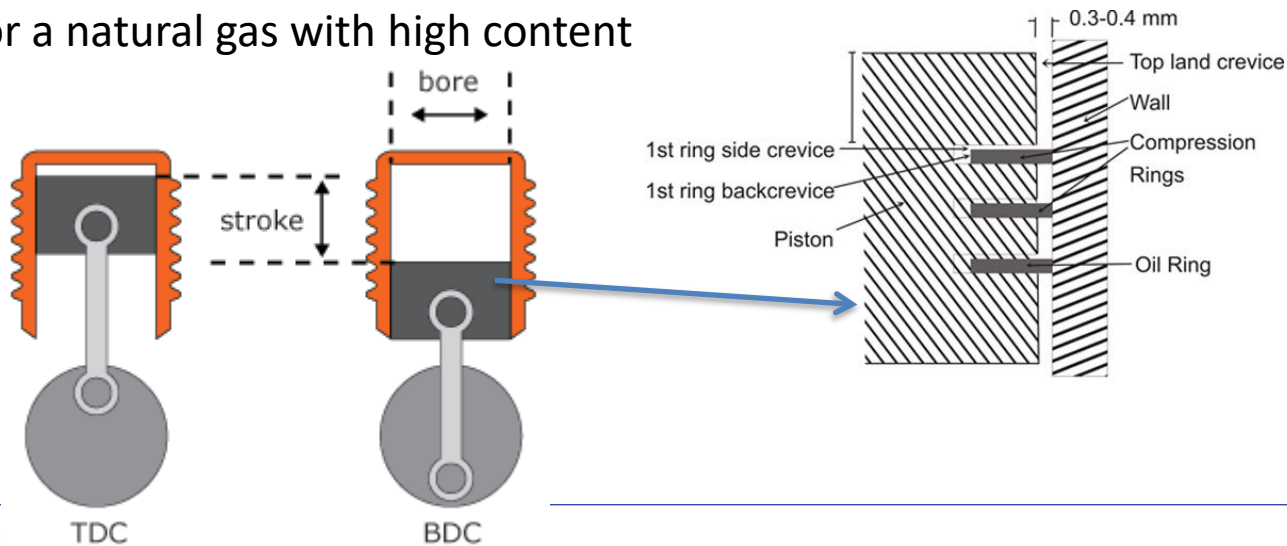


Laminar Flame Speed and reactants flow



#18 Imagine you are using LPG in a 4 cylinder, 1.4 liter internal combustion engine, compression ratio 12, bore=stroke, equipped with an exhaust aftertreatment system, a three-way catalytic converter, TWC. Assume a spherical centered flame front, cold start and hot regime.

- LPG has a high octane number. Identify the type of combustion constant volume or constant pressure?
- Estimate the dimensions of the combustion chamber (assume bore=stroke).
- How much time do you estimate will be the combustion duration?.
- Discuss HC (non-methane volatile organic compounds) formation near the oil rings where the temperature is 100°C . What would be the function of the TWC
- Repeat for a natural gas with high content





Ideal Otto Cycle p-V diagram

Glenn
Research
Center

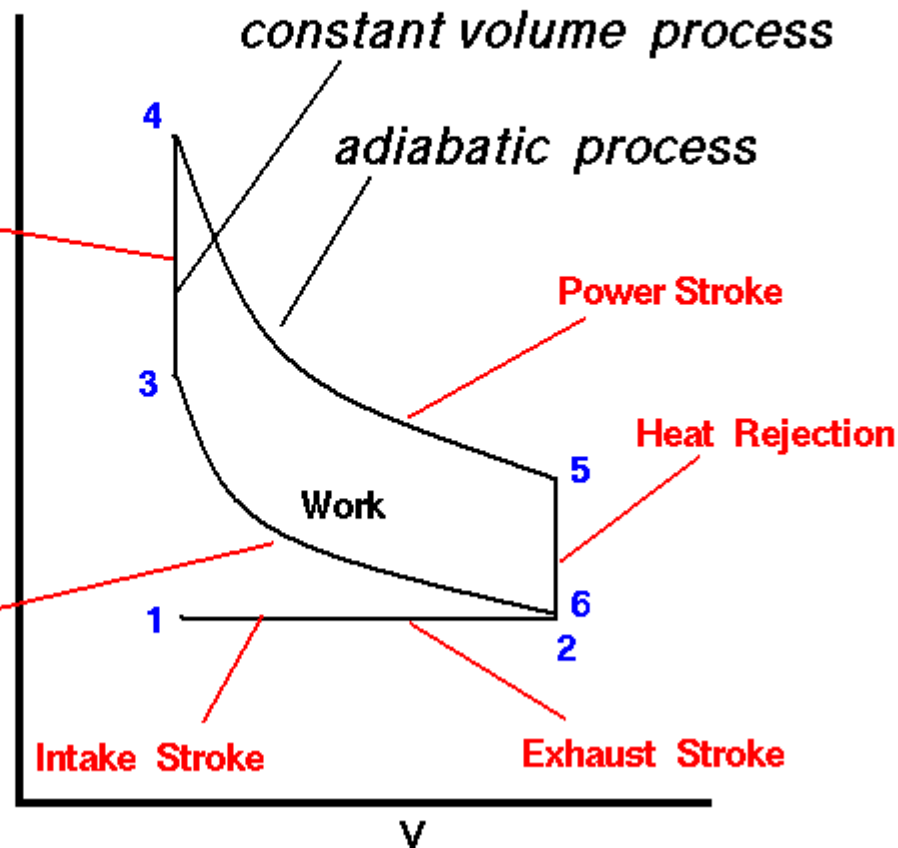
V = Volume
 p = pressure

Combustion Process

Point 1 - 1 atm
 Point 3 - 1000 kPa
 Point 4 - 2750 kPa

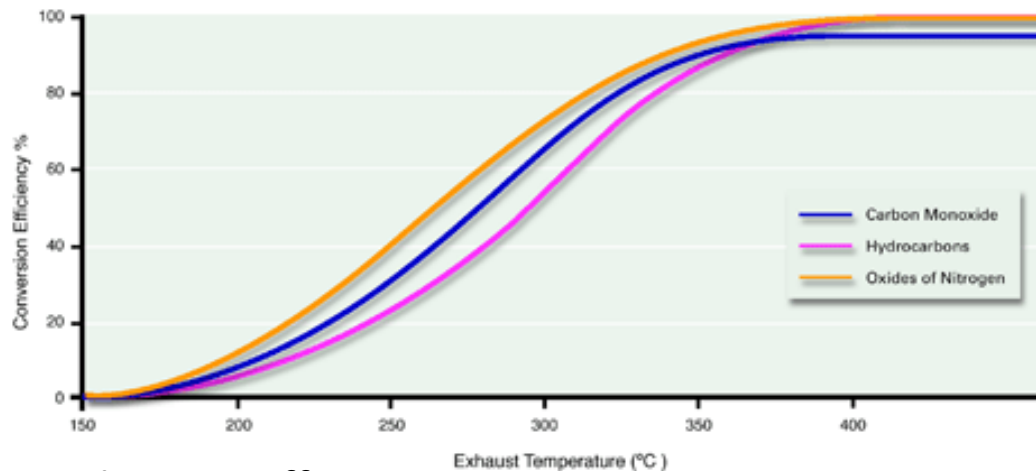
Compression Stroke

e.g. pg 385 Internal
combustion engine
fundamentals



P#19 A mixture of methane gas and air at 25°C and 1 atm is burned in a water heater at 100% theoretical air. The mass flow rate of methane is 1.15 kg/h. The exhaust gas temperature was measured to be 500 °C and approximately 1 atm and is subjected to exhaust aftertreatment. The volumetric flow rate of cold water (at 22 °C) to the heater is 4 L/min. Flue gas is equipped with a TWC.

Effect of temperature on the operation of a three-way catalytic converter (Lambda= 1)

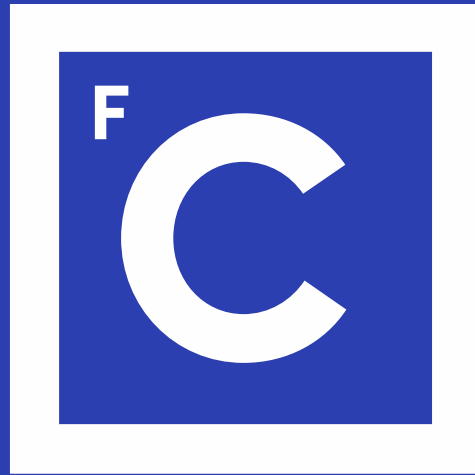


- Determine the combustion efficiency.
- Calculate the temperature of the hot water if the heat exchanger were to have an efficiency of 1.0, i.e., perfect heat transfer.
- Consider the following concentrations of emissions at the combustion products: 5000 ppm NO. Estimate the NO exhaust gas emissions in g/h.

P#20 The following sentences are true or false?

- a) The molar mass of an ideal mixture is equal to the sum of each species molar mass weighted by its molar fractions.
- b) In a rich mixture $\phi > 1$.
- c) The adiabatic flame temperature, at constant pressure, increases with the increase in the reactants temperature.
- d) At 3000 K H_2 is more likely to dissociate to its monoatomic form, than N_2 .
- e) In 2 adiabatic recipients, different dimensions, it was introduced the same mass of air and fuel at T_{amb} . After ignition, and once reached the equilibrium, the dissociation is higher in the smallest recipient.

Obrigado



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